



# Isotopic evidence for alteration of nitrous oxide emissions and producing pathways contribution under nitrifying conditions

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**Abstract.** Nitrous oxide (N<sub>2</sub>O) emissions by a nitrifying biofilm reactor were investigated with N<sub>2</sub>O isotopocules. The site preference of N<sub>2</sub>O (<sup>15</sup>N-SP) indicated the contribution of producing and consuming pathways in response to changes in oxygenation level (from 0 to 21 % O<sub>2</sub> in the gas mix), temperature (from 13.5 to 22.3 °C), and ammonium concentrations (from 6.2 to 62.1 mg N L<sup>-1</sup>). Nitrite reduction, either nitrifier-denitrification or heterotrophic denitrification, was the main N<sub>2</sub>O producing pathway under the tested conditions. Nitrite oxidation rates decreased as compared to ammonium oxidation rates at temperatures above 20 °C and sub-optimal oxygen levels, increasing N<sub>2</sub>O production by the nitrite reduction pathway. Below 20 °C, a difference in temperature sensitivity between hydroxylamine and ammonium oxidation rates is most likely responsible for an increase in the N<sub>2</sub>O production via the hydroxylamine oxidation pathway (nitrification). A negative correlation between the reaction kinetics and the apparent isotope fractionation was additionally shown from the variations of δ<sup>15</sup>N and δ<sup>18</sup>O values of N<sub>2</sub>O produced from ammonium.

## 1 Introduction

Nitrogen (N) cycling lies on numerous biological processes exploited and altered by anthropic activities (Bothe et al., 2007). One of the major issues related to N cycle alteration is the production of nitrous oxide (N<sub>2</sub>O) a potent ozone-depleting and greenhouse gas whose emissions exponentially increased during the industrial era (Crutzen et al., 1979; IPCC, 2014; Ravishankara et al., 2009). Wastewater resource recovery facilities (WRRFs) contribute to about 3 % of annual global anthropogenic N<sub>2</sub>O sources (ca. 6.7 ± 1.3 Tg N-N<sub>2</sub>O in 2011; IPCC, 2014); with 0 to 25 % of the influent nitrogen loads emitted as N<sub>2</sub>O (Law et al., 2012b). The challenges in mitigation of these emissions rely on the understanding of the producing processes and their controls.



Two microbial processes are responsible for the production of  $N_2O$  (nitrification and denitrification), with only one of these capable of consuming it (Kampschreur et al., 2009) (denitrification; Fig. 1a). Nitrification is the oxidation of ammonium to nitrite ( $NO_2^-$ ) via the intermediate hydroxylamine ( $NH_2OH$ ) conducted by ammonia oxidizers and the subsequent oxidation of  $NO_2^-$  to nitrate ( $NO_3^-$ ) by nitrite oxidizers. During nitrification,  $N_2O$  can be produced as reaction side-product from hydroxylamine oxidation by biotic, abiotic or hybrid processes (Caranto et al., 2016; Heil et al., 2015; Terada et al., 2017). Heterotrophic denitrification and nitrifier-denitrification produce  $N_2O$  from nitrite reduction conducted by denitrifiers and ammonium oxidizers, respectively.

Temperature, electron donor and acceptor concentrations have been identified to control the  $N_2O$  emission from WRRFs (Bollon et al., 2016; Kampschreur et al., 2009; Tallec et al., 2006; Wunderlin et al., 2012). These variables may induce  $N_2O$  accumulation due to inhibition or disturbance of enzyme activity (Betlach and Tiedje, 1981; Kim et al., 2008; Otte et al., 1996). In addition to this, the different  $N_2O$  producing processes, nitrification, nitrifier-denitrification or heterotrophic denitrification, are rarely observed independently from each other in heterogeneous environments like wastewater. However, the understanding of the influence that environmental conditions have on the balance between these processes and the  $N_2O$  producing pathways remain to a large extent unexplored.

In order to decipher  $N_2O$  producing/consuming pathways, the analysis of  $N_2O$  isotopocules, molecules that only differ in either the number or position of isotopic substitutions, has been applied (Koba et al., 2009; Sutka et al., 2006) (Figs. 1b-d). The isotope composition of substrates and fractionation mechanisms influence both nitrogen and oxygen isotope ratios of  $N_2O$  (reported as  $\delta^{15}N$  and  $\delta^{18}O$ , respectively, Fig. 1b). Basically, the oxygen atom in the  $N_2O$  molecule produced by hydroxylamine oxidation originates from atmospheric dissolved oxygen with  $\delta^{18}O$  of 23.5 ‰ (Andersson and Hooper, 1983; Hollocher et al., 1981; Kroopnick and Craig, 1972), while the oxygen atom in  $N_2O$  produced by nitrite reduction originates from nitrite that has undergone oxygen-exchange with water (Kool et al., 2007; Snider et al., 2012). Nonetheless, the  $\delta^{18}O$ - $N_2O$  resulting from the nitrite reduction conducted by the nitrifiers ranges from 13 to 35 ‰ (Snider et al., 2012). In contrast, the  $N_2O$  produced by the denitrifiers through the nitrite reduction pathway has  $\delta^{18}O$  over 35 ‰ (Snider et al., 2013). However, the O-exchange between the  $N_2O$  precursors and water can decrease it to values below 35 ‰ (Snider et al., 2015). Therefore, the  $\delta^{18}O$  alone does not enable differentiation between the  $N_2O$  producing pathways.

In combination with  $\delta^{18}O$ , the  $\delta^{15}N$ - $N_2O$  allows to identify the  $N_2O$  producing pathways (Fig. 1b). However, the isotope fractionations (or isotope effects) largely influence the  $\delta^{15}N$ - $N_2O$  due to wide variations between and within the reactions involved in the nitrogen cycle (Denk et al., 2017). The isotopic fractionations result from the difference in equilibrium constant (abiotic process) or reaction rate (biotic process) observed between the heavier and lighter isotopes. The net isotope effects ( $\Delta$ ) approximated from the difference between  $\delta^{15}N$  of product and substrate characterize the production of compounds resulting from sequential or branched reactions and have been recently reviewed (Denk et al., 2017; Toyoda et al., 2017). So far, only two estimates of the net isotope effect of  $N_2O$  production by ammonium oxidation via hydroxylamine of -46.9 and -32.6 ‰ have been proposed (Sutka et al., 2006; Yamazaki et al., 2014). These values are imbricated between -52.8 and -6 ‰, the range



of net isotope effects related to the  $\text{N}_2\text{O}$  production through nitrite reduction performed by nitrifiers or denitrifiers (Lewicka-  
65 Szczebak et al., 2014; Sutka et al., 2008).

Similarly to isotope ratios, the nitrogen isotopomer site preference ( $^{15}\text{N}$ -SP), the difference between the relative abundances  
of  $\text{N}_2\text{O}$  molecules enriched in the central ( $\text{N}^\alpha$ ) position and in the terminal ( $\text{N}^\beta$ ) position, differ according to  $\text{N}_2\text{O}$  producing  
pathway (Figs. 1c and d). During heterotrophic or nitrifier-denitrification the  $^{15}\text{N}$ -SP of  $\text{N}_2\text{O}$  produced from nitrate or nitrite  
70 ranges from -10.7 to 0.1 ‰, while ranging from 13.1 to 36.6 ‰ when  $\text{N}_2\text{O}$  results from hydroxylamine oxidation (Frame and  
Casciotti, 2010; Jung et al., 2014; Sutka et al., 2006; Yamazaki et al., 2014). Finally,  $\text{N}_2\text{O}$  reduction to  $\text{N}_2$  by heterotrophic  
denitrifiers increases the values of  $\delta^{15}\text{N}$ ,  $\delta^{18}\text{O}$  and  $^{15}\text{N}$ -SP of residual  $\text{N}_2\text{O}$  with specific pairwise ratios (Jinuntuya-Nortman et  
al., 2008; Webster and Hopkins, 1996; Yamagishi et al., 2007).

Nitrogen and oxygen isotope ratios of  $\text{N}_2\text{O}$  are often disregarded, due to lower potential for  $\text{N}_2\text{O}$  source identification as  
compared to  $^{15}\text{N}$ -SP. However, we believe that the use of both isotope approaches should strengthen the conclusions from  $^{15}\text{N}$ -  
75 SP and reveal additional isotope effects (Fig. 1).

The aim of the current study is to improve our understanding regarding the effects of key environmental variables (oxygenation,  
temperature,  $\text{NH}_4^+$  concentrations) on  $\text{N}_2\text{O}$  production and emission rates. More specifically using nitrogen and oxygen isotope  
ratios as well as  $^{15}\text{N}$ -SP of  $\text{N}_2\text{O}$  should allow deciphering the different producing and consuming pathways under these different  
conditions. In order to achieve this, the nitrifying biomass of a submerged fixed-bed biofilm reactor was investigated. The  
80 research questions addressed are: i) Does the nitrifying biomass emit  $\text{N}_2\text{O}$  and what are the producing pathways at play?; ii)  
Do oxygenation, temperature, and  $\text{NH}_4^+$  concentration alter the  $\text{N}_2\text{O}$  emissions, and what are the involved processes. We  
hypothesize that the isotope signature of  $\text{N}_2\text{O}$  allows identifying the  $\text{N}_2\text{O}$  origins and the assessment of pathway contribution  
to  $\text{N}_2\text{O}$  emissions. The results of this study should improve the mechanistic understanding as well as improved prediction of  
 $\text{N}_2\text{O}$  emissions from WRRFs, currently suffering from high uncertainty.

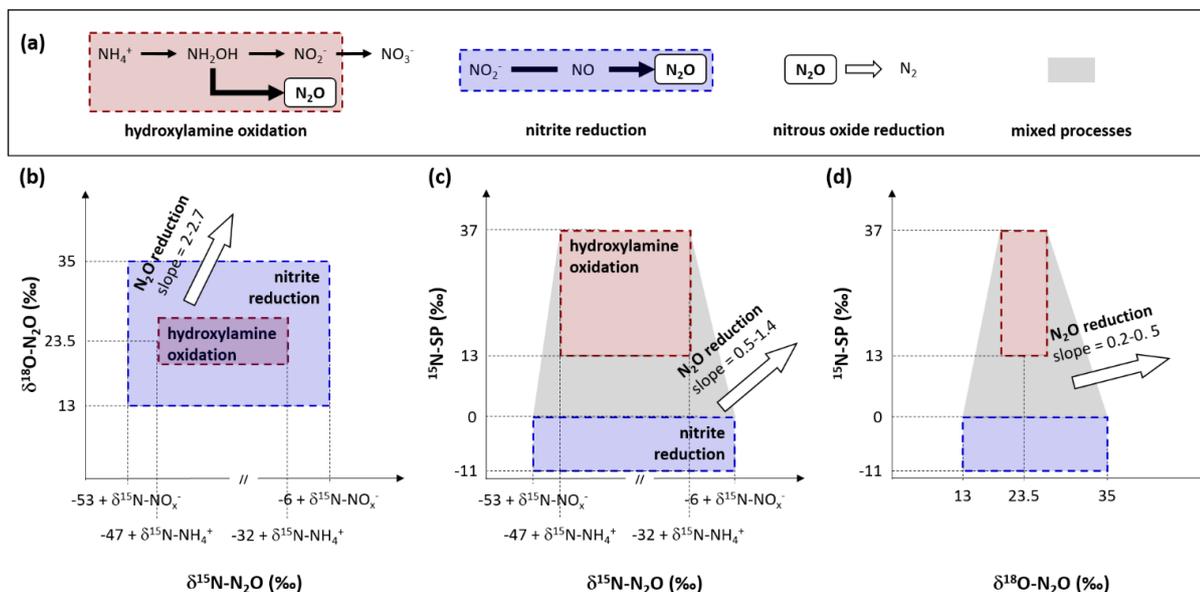


Figure 1: N<sub>2</sub>O producing and consuming pathways at play during nitrification and denitrification.

## 85 2 Material and methods

### 2.1 Experimental setup for nitrifying experiments

Experiments were carried out with colonized polystyrene beads (diameter 4 mm) sampled from the nitrification biologically active filters (BAF) of a domestic WRRF (Seine Centre, France). In this WRRF, wastewater (240,000 m<sup>3</sup> d<sup>-1</sup>) passes through a pre-treatment stage, followed by a physicochemical decantation, and tertiary biological treatment. The latter is composed of three biofiltration processes; (i) carbon elimination (24 Biofor®), (ii) nitrification (29 Biostyr®), and (iii) denitrification (12 Biofor®). Nitrifying Biostyrs® are submerged fixed-bed biofilm reactors with a unitary section of 111 m<sup>2</sup> and a filter bed of 3 m high. This unit is operated to receive a nominal load of 0.7 kg NH<sub>4</sub><sup>+</sup>-N m<sup>-3</sup> d<sup>-1</sup>.

A lab-scale reactor with a working volume of 9.9 L (colonized Biostyrene® beads and interstitial volume) and a headspace of 1.4 L was operated in continuous down-flow counter-current mode for seven weeks. Mass flow meters (F-201CV, Bronkhorst, France) sustained the inflow gas rate at 0.5 L min<sup>-1</sup>. A peristaltic pump (R3425H12B, Sirem, France) pumped feeding solution from a feeding tank into the reactor at 0.2 L min<sup>-1</sup>, in order to maintain a hydraulic retention time (HRT) of 27.8 ± 0.6 min. A water jacket monitored by a cryogenic regulator (WK 500, Lauda, Germany) controlled the reactor temperature. The feeding solution consisted of ammonium chloride (NH<sub>4</sub>Cl) as substrate, monobasic potassium phosphate (KH<sub>2</sub>PO<sub>4</sub>) as phosphorus source for bacterial growth, and sodium hydrogen carbonate (NaHCO<sub>3</sub>) as pH buffer and inorganic carbon source in 100 or 100 150 L of tap water.



The influence of environmental conditions on the ammonium oxidation rates and the N<sub>2</sub>O emissions from various combinations of oxygenation levels, temperatures and ammonium concentrations were tested in twenty-four experiments (Tables 1 and S1). The oxygenation tests consisted of mixing compressed air and pure nitrogen gas to reach 0 to 21 % O<sub>2</sub> in the gas mixture (Fig. S1a). They were performed at five substrate concentrations and at a temperature between 19.2 and 20.6 °C. The temperature tests consisted of cooling the feeding solution directly in the feeding tank (22.3 to 13.5 °C), with an inflow ammonium concentration of 19.9-21.1 mg NH<sub>4</sub><sup>+</sup>-N L<sup>-1</sup>. At temperatures ranging from 18.8 to 19.9 °C, the ammonium concentration tests consisted of an increase (6.2, 28.6 and 62.1 mg NH<sub>4</sub><sup>+</sup>-N L<sup>-1</sup>) and a decrease (56.1, 42.9, 42.7 and 20.2 mg NH<sub>4</sub><sup>+</sup>-N L<sup>-1</sup>) in the NH<sub>4</sub><sup>+</sup> concentrations in the feeding solution. An optimal oxygenation level was imposed for both tests (Figs. S1b and c). Sampling started after at least one hydraulic retention time (28 ± 1 min).

110 **Table 1. Ranges of environmental conditions tested.**

tests	inflow [NH <sub>4</sub> <sup>+</sup> ] <i>mg N L<sup>-1</sup></i>	inflow gas rate <i>L min<sup>-1</sup></i>	O <sub>2</sub> in gas mixture %	temperature °C
oxygenation	20.2 - 37.3	0.4 - 0.57	0 - 21	19.2 - 20.6
temperature	20.2 - 21.1	0.5	21	13.5 - 22.3
inflow [NH <sub>4</sub> <sup>+</sup> ]	6.2 - 62.1	0.5, 0.57	21	19.0 - 20.3

## 2.2 Reactor monitoring, sampling and concentrations analysis

Dissolved oxygen, temperature (Visiferm DO Arc 120, Hamilton, Switzerland) and pH (H8481 HD, SI Analytics, France) were continuously measured at the top of the reactor and data were recorded at 10 second intervals. The N<sub>2</sub>O concentration was continuously analyzed by an infrared photometer (Rosemount™ X-STREAM X2GP, Emerson, Germany) in outflow reactor gas after drying through a condenser and a hydrophobic gas filter (0.2 μm). Minute averages are used for monitored data hereafter. Gas samples were taken for N<sub>2</sub>O isotopic signature determination by outlet gas pipe derivation into a sealed glass vial of 20 ml. The vial was first flushed with the sampling gas for > 45 sec prior to 1-5 min sampling. Gas samples were then stored in the dark at room temperature until analysis.

The feeding solutions were characterized from 1 to 5 samples collected in the feeding tank. For each tested condition, the outflow was characterized within 5 days from 1 to 14 samples immediately filtered through a 0.2 μm syringe filter and stored at 4 °C. Ammonium was analyzed using the Nessler colorimetric method, according to AFNOR NF T90-015 (DR 2800, Hach, Germany). Nitrite and nitrate were measured by ionic chromatography (IC25, Dionex, USA).

## 2.3 Stable isotope measurements

Atmospheric N<sub>2</sub> and Vienna Standard Mean Ocean Water (VSMOW) are the references used for the nitrogen and oxygen isotopes ratios, respectively, expressed in the conventional δ-notation, in per-mil (‰). Nitrogen and oxygen isotope ratios of



nitrate and nitrite were determined separately following a modified protocol of McIlvin and Altabet (McIlvin and Altabet, 2005; Semaoune et al., 2012). Nitrogen isotope ratios of ammonium were determined following the protocol of Zhang et al. (2007). These methods consist in the conversion of the substrate (ammonium or nitrite or nitrate) into dissolved  $N_2O$ . The  $\delta^{15}N$  and  $\delta^{18}O$  values of  $N_2O$  and  $^{15}N$  site preference ( $^{15}N$ -SP) values were determined using an isotope ratio mass spectrometer (IRMS, DeltaVplus; Thermo Scientific) in continuous-flow with a purge and trap system coupled with a Finnigan GasBench II system (Thermo Scientific). The method was calibrated with combination of nitrate or ammonium standards (USGS-32,  $\delta^{15}N-NO_3^- = 180$  ‰,  $\delta^{18}O-NO_3^- = 25.7$  ‰; USGS-34,  $\delta^{15}N-NO_3^- = -1.8$  ‰,  $\delta^{18}O-NO_3^- = -27.9$  ‰ and USGS-35  $\delta^{15}N-NO_3^- = 2.7$  ‰,  $\delta^{18}O-NO_3^- = 57.5$  ‰; or IAEA-N1,  $\delta^{15}N-NH_4^+ = 0.4$  ‰, IAEA-305A,  $\delta^{15}N-NH_4^+ = 39.8$  ‰, USGS-25,  $\delta^{15}N-NH_4^+ = -30.4$  ‰). Linearity of the analysis was checked with international standards (IAEA-NO-3,  $\delta^{15}N-NO_3^- = 4.7$  ‰,  $\delta^{18}O-NO_3^- = 25.6$  ‰; or IAEA-N2,  $\delta^{15}N-NH_4^+ = 20.3$  ‰). The precision was 0.8 ‰, 1.5 ‰ and 2.5 ‰ for  $\delta^{15}N$ ,  $\delta^{18}O$ , and  $^{15}N$ -SP, respectively.

## 2.4 Data processing and statistics

The effects of environmental conditions on nitrification were assessed from 4 indices. The ammonium oxidation rate (AOR) was estimated in each experiment for time  $\geq 1$  HRT from the difference between influent and effluent  $NH_4^+$  concentrations multiplied by the liquid flow rate ( $kg\ NH_4^+-N\ m^{-3}\ d^{-1}$ ). The nitrification efficiency was defined as the ratio between AOR and influent ammonium load. The  $N_2O$  emission rate ( $N_2O$ -ER) was calculated by multiplying the measured  $N_2O$  concentration by the gas flow rate ( $mg\ N_2O-N\ min^{-1}$ ). The  $N_2O$  emission factor ( $N_2O$ -EF) was defined as the ratio between  $N_2O$ -ER and AOR (% of oxidized  $NH_4^+-N$ ).

Statistical analysis were performed using the R software (R Core Team, 2014). The value of 0.05 was used as significance level for spearman correlations (*cor.test* function) and linear regressions (*lm* function). *Adjusted  $r^2$*  was provided as  *$r^2$*  for the latter.

## 2.5 Estimation of nitrogen isotope ratio in $N_2O$

As shown in Fig. 1, the pairwise relationships between  $\delta^{15}N$ ,  $\delta^{18}O$  and  $^{15}N$ -SP assist the determination of the producing and consuming pathways at play. The N atoms that compose the  $N_2O$  molecule originate from  $NH_4^+$  molecules when produced by hydroxylamine oxidation, while originating from the N atoms of  $NO_3^-$  or  $NO_2^-$  molecules when produced by nitrite reduction ( $NO_2^-$  molecules). However, the nitrogen isotope ratio of  $N_2O$  does not equal those of its substrates as it depends on isotope effects associated to each reaction step of  $N_2O$  producing process.

Several equations enable to approximate the isotope effect and its effect on the isotope ratios of substrate and product pools involved in a reaction. These equations vary according to the assumptions made on the system boundaries (Denk et al., 2017). The nitrifying reactor used in this study can be described as an open-system continuously through by an infinite substrate pool with constant isotopic composition. A small amount of the infinite substrate pool is transformed into a product pool or a



residual substrate pool when flowing through the system. Therefore, the N isotope ratios of the residual substrate pool can be approximated from the following Eq. (1) (Denk et al., 2017; Fry, 2006):

$$\delta^{15}\text{N-NH}_4^+{}_{,\text{out}} \approx \delta^{15}\text{N-NH}_4^+{}_{,\text{in}} - (1 - f) \times \varepsilon_{\text{ao}}, \quad (1)$$

160 Where  $f$  is the remaining substrate fraction leaving the reactor (i.e. remaining fraction of ammonium), ranging from 0 to 1 (0-100 in %), and  $\varepsilon_{\text{ao}}$  the N isotope enrichment factor associated with ammonium oxidation. In their review, Denk et al. (2017) reported a mean value of  $-29.6 \pm 4.9$  ‰ for  $\varepsilon_{\text{ao}}$ . Therefore,  $\delta^{15}\text{N}$  is higher for residual than initial substrate pool ( $\delta^{15}\text{N-NH}_4^+{}_{,\text{in}} < \delta^{15}\text{N-NH}_4^+{}_{,\text{out}}$ ; where ‘in’ and ‘out’ represent inflow and outflow, respectively). Consequently, the pool of product is depleted in heavier isotope (i.e. nitrite and nitrate hereafter defined as  $\text{NO}_x^-$  pool;  $\delta^{15}\text{N-NO}_x^-{}_{,\text{in}} > \delta^{15}\text{N-NO}_x^-{}_{,\text{out}}$ ). It can be estimated from  
 165 Eq. (2):

$$\delta^{15}\text{N-NO}_x^-{}_{,\text{p}} \approx \delta^{15}\text{N-NH}_4^+{}_{,\text{in}} + f \times \varepsilon_{\text{ao}}, \quad (2)$$

Where  $\delta^{15}\text{N-NO}_x^-{}_{,\text{p}}$  is the nitrogen isotope ratio of the product pool produced by nitrification. The nitrogen isotope ratio of the overall  $\text{NO}_x^-$  exiting the reactor ( $\delta^{15}\text{N-NO}_x^-{}_{,\text{out}}$ ), which results of mixing between initial and produced  $\text{NO}_x^-$  pools, can be estimated from Eqs. (3) and (4):

$$170 \quad \delta^{15}\text{N-NO}_x^-{}_{,\text{in}} = \frac{(\delta^{15}\text{N-NO}_2^-{}_{,\text{in}} \times [\text{NO}_2^-]_{\text{in}} + \delta^{15}\text{N-NO}_3^-{}_{,\text{in}} \times [\text{NO}_3^-]_{\text{in}})}{([\text{NO}_3^-]_{\text{in}} + [\text{NO}_2^-]_{\text{in}})}, \quad (3)$$

$$\delta^{15}\text{N-NO}_x^-{}_{,\text{out}} \approx \frac{(\delta^{15}\text{N-NO}_x^-{}_{,\text{in}} \times ([\text{NO}_3^-]_{\text{in}} + [\text{NO}_2^-]_{\text{in}}) + \delta^{15}\text{N-NO}_x^-{}_{,\text{p}} \times f \times [\text{NH}_4^+]_{\text{in}})}{([\text{NO}_3^-]_{\text{in}} + [\text{NO}_2^-]_{\text{in}} + f \times [\text{NH}_4^+]_{\text{in}})}, \quad (4)$$

Whatever the considered system, the net isotope effect of sequential or branched reactions can be approximated from the  $\Delta$  method that consists in the difference between  $\delta^{15}\text{N}$  of product and substrate (Denk et al., 2017). Therefore, the nitrogen isotope ratio of  $\text{N}_2\text{O}$  produced by hydroxylamine oxidation or nitrite reduction can be estimated from Eq. (5), with the underlying  
 175 assumptions that the initial amount of  $\text{N}_2\text{O}$  is negligible as compared to the amount of produced  $\text{N}_2\text{O}$ .

$$\delta^{15}\text{N-N}_2\text{O} \approx \delta^{15}\text{N}_s + \Delta, \quad (5)$$

Where  $\delta^{15}\text{N}_s$  is the nitrogen isotope ratio of  $\text{N}_2\text{O}$  substrate, which can range between the nitrogen isotope ratios measured or estimated for inflow and outflow  $\text{NH}_4^+$  and  $\text{NO}_x^-$  (Eqs. (1-4)). Net isotope effects ( $\Delta$ ) from literature were used for each  $\text{N}_2\text{O}$  producing pathway (Denk et al., 2017; Toyoda et al., 2017).

### 180 3 Results and Discussion

Changes in pH, ammonium, nitrite and nitrate concentrations confirmed nitrifying activity in the reactor system (Text S1, Table S2, Fig. S2). Over the range of tested conditions, the ratio between ammonium oxidation rate and influent ammonium concentrations ranged from 10 to 82 %, never exceeding 40 % for suboptimal nitrifying conditions imposed during oxygenation



and temperature tests. Within the tested oxygen, temperature and ammonia conditions, the resulting range of ammonium  
185 oxidation rates, N<sub>2</sub>O emission rates and factors decreased in the order ammonium concentration, oxygenation level and  
temperature.

### 3.1 Isotope composition ranges of N<sub>2</sub>O produced by hydroxylamine oxidation and nitrite reduction

Ranges of  $\delta^{15}\text{N}$  for N<sub>2</sub>O produced by different processes were hypothesized from Eqs. (1-5) for pairwise relationships with  
reviewed data of  $\delta^{18}\text{O}$  and  $^{15}\text{N}$ -SP. To this aim, measurements of isotope ratios of the different nitrogen species were required.  
190 The  $\delta^{15}\text{N}$  of inflow ammonium, nitrite and nitrate were  $-3 \pm 0.1 \text{ ‰}$  ( $n = 3$ ),  $-15 \pm 0.1 \text{ ‰}$  ( $n = 2$ ),  $6.9 \pm 0.3 \text{ ‰}$  ( $n = 3$ ), respectively  
during ammonium concentration experiments (Fig. S2). The  $\delta^{15}\text{N}$  of outflowing  $\text{NH}_4^+$  and  $\text{NO}_x^-$  were estimated from Eqs. (1-4)  
with  $f = 0$  or  $1$ ,  $\epsilon_{\text{ao}} = -30 \text{ ‰}$ , the highest  $[\text{NH}_4^+]_{\text{in}}$  ( $62.1 \text{ mg N L}^{-1}$ ) and the lowest  $[\text{NO}_x^-]_{\text{in}}$  ( $1.4 \text{ mg N L}^{-1}$ ). They ranged from  $-3$   
to  $27 \text{ ‰}$  and from  $-32$  to  $7 \text{ ‰}$ , respectively.

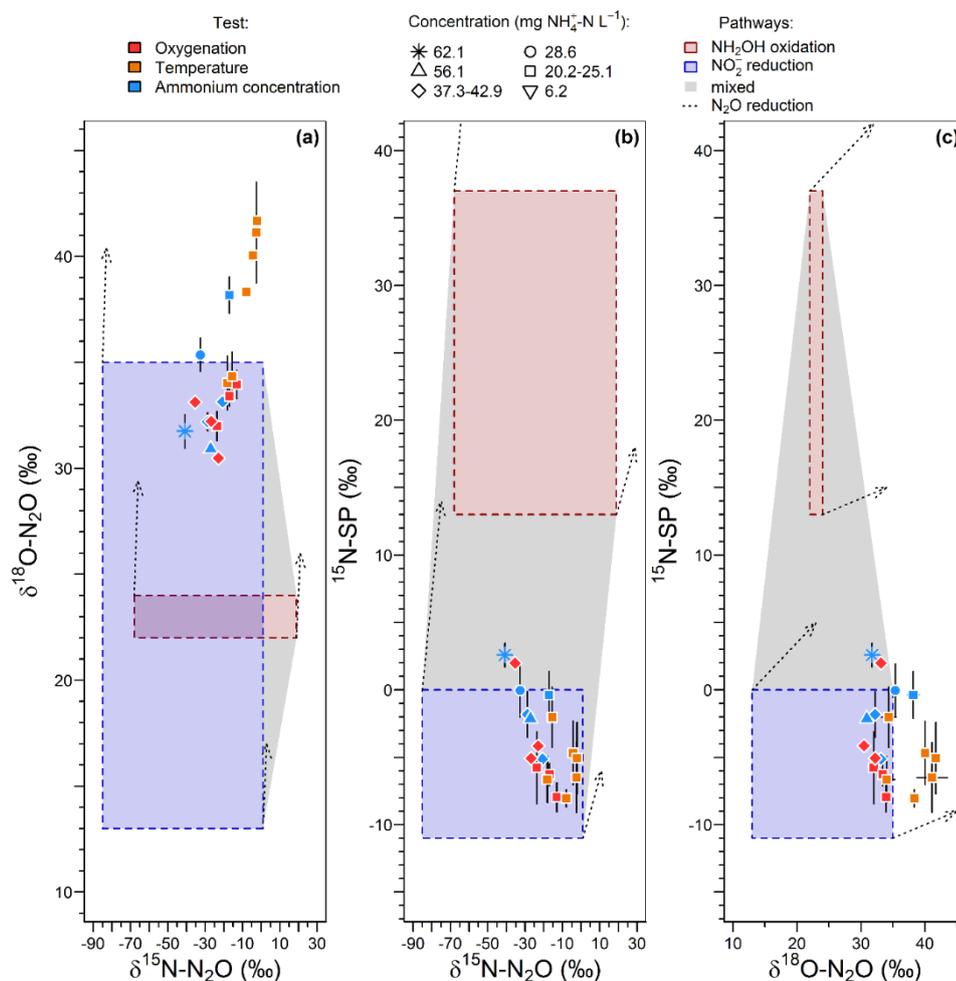
Prior to pairwise comparisons with  $\delta^{18}\text{O}$  and  $^{15}\text{N}$ -SP, ranges of  $\delta^{15}\text{N}$  values for N<sub>2</sub>O produced by the hydroxylamine oxidation  
195 and nitrite reduction pathways were estimated from Eq. (5). The net isotope effect of N<sub>2</sub>O production by ammonium oxidation  
via hydroxylamine can be estimated by combining the isotope effects of ammonium oxidation and hydroxylamine oxidation  
to N<sub>2</sub>O. The net isotope effect associated to the ammonium oxidation to nitrite ranges from  $-38.2$  to  $-14.2 \text{ ‰}$  (Casciotti et al.,  
2003) and can approximate the nitrogen isotope ratio of hydroxylamine transitory produced. The isotope effect related to  
hydroxylamine oxidation to N<sub>2</sub>O ranging from  $-26.3$  to  $5.7 \text{ ‰}$  (Sutka et al., 2003, 2006), the net isotope effect of N<sub>2</sub>O  
200 production by ammonium oxidation via hydroxylamine can range from  $-64.5 \text{ ‰}$  ( $-26.3 + (-38.2)$ ) to  $-8.5 \text{ ‰}$  ( $5.7 + (-14.2)$ ).  
This method provided a broad range of  $\delta^{15}\text{N}$  values, from  $-68$  to  $19 \text{ ‰}$ , for N<sub>2</sub>O produced by hydroxylamine oxidation that  
encompassed the values proposed by others ( $-46.9$  and  $-32.6 \text{ ‰}$ ; Sutka et al., 2006; Yamazaki et al., 2014).

A higher net nitrogen isotope effect for nitrite reduction than hydroxylamine oxidation pathway was observed for N<sub>2</sub>O  
production (Figs. 2a and b). Prior being reduced to N<sub>2</sub>O through the nitrite reduction pathway,  $\text{NO}_x^-$  was mainly derived from  
205 ammonium oxidation in the nitrifying system (Eqs. (1-4)). Consequently, the  $\delta^{15}\text{N}$  of N<sub>2</sub>O produced by nitrite reduction ranged  
from  $-85 \text{ ‰}$  ( $-53 + (-32)$ ) to  $1 \text{ ‰}$  ( $-6 + 7$ ). This is consistent with previous findings reporting  $\delta^{15}\text{N}$ -N<sub>2</sub>O between  $-112$  and  $-48 \text{ ‰}$   
for nitrifier-denitrifying systems (Mandernack et al., 2009; Pérez et al., 2006; Yamazaki et al., 2014; Yoshida, 1988). However,  
a similar range of nitrite-derived  $\delta^{15}\text{N}$ -N<sub>2</sub>O is suggested for nitrifiers and denitrifiers, because ammonium oxidation influences  
both processes in the system used in this study.

210 Pairwise comparisons of  $\delta^{15}\text{N}$ ,  $\delta^{18}\text{O}$  and  $^{15}\text{N}$ -SP estimates of the different experiments are presented in Fig. 2. These  
comparisons provided ranges of plausible isotope compositions for N<sub>2</sub>O produced by nitrifying or denitrifying bacteria through  
the hydroxylamine oxidation and nitrite reduction pathways (red and blue boxes, respectively). The measured N<sub>2</sub>O isotope  
compositions were compared to these estimates to identify the N<sub>2</sub>O producing and consuming pathways likely at play in  
oxygenation, temperature, and ammonium concentration tests.



215 This approach suggests that the nitrite reduction pathway was the main contributor to the N<sub>2</sub>O emissions. Heterotrophic  
 denitrification likely influenced the N<sub>2</sub>O emissions, as shown by oxygen isotope ratios higher than 35 ‰ (Snider et al., 2013)  
 (Figs. 2a and c). However, this conclusion depends highly on δ<sup>18</sup>O-N<sub>2</sub>O ranges. Furthermore, the application of atmospheric  
 oxygen δ<sup>18</sup>O (23.5 ‰; Kroopnick and Craig, 1972) to estimate the oxygen isotope ratio of N<sub>2</sub>O produced by hydroxylamine  
 oxidation remains uncertain since respiratory activity and air stripping might drive isotopic fractionations and increase the  
 220 δ<sup>18</sup>O of residual dissolved oxygen (Nakayama et al., 2007). To date, the oxygen isotope fractionation related to air stripping is  
 lacking. Note that this estimate relies on the assumption that there is no accumulation of NH<sub>2</sub>OH and that its oxidation to N<sub>2</sub>O  
 occurs before or independently of its oxidation to NO<sub>2</sub><sup>-</sup>.



**Figure 2: Interpretation maps of the isotope signature of N<sub>2</sub>O. Schematic maps of (a) δ<sup>15</sup>N-δ<sup>18</sup>O, (b) δ<sup>15</sup>N-<sup>15</sup>N-SP, and (c) δ<sup>18</sup>O-<sup>15</sup>N-SP. The red and blue squares show the range of the data for N<sub>2</sub>O produced by ‘hydroxylamine oxidation’ and ‘nitrite reduction’, respectively. The shaded area represents mixing of N<sub>2</sub>O produced by these pathways. The N<sub>2</sub>O reduction increases δ<sup>15</sup>N, δ<sup>18</sup>O, and <sup>15</sup>N-SP with slopes characterizing the pairwise relationships.**



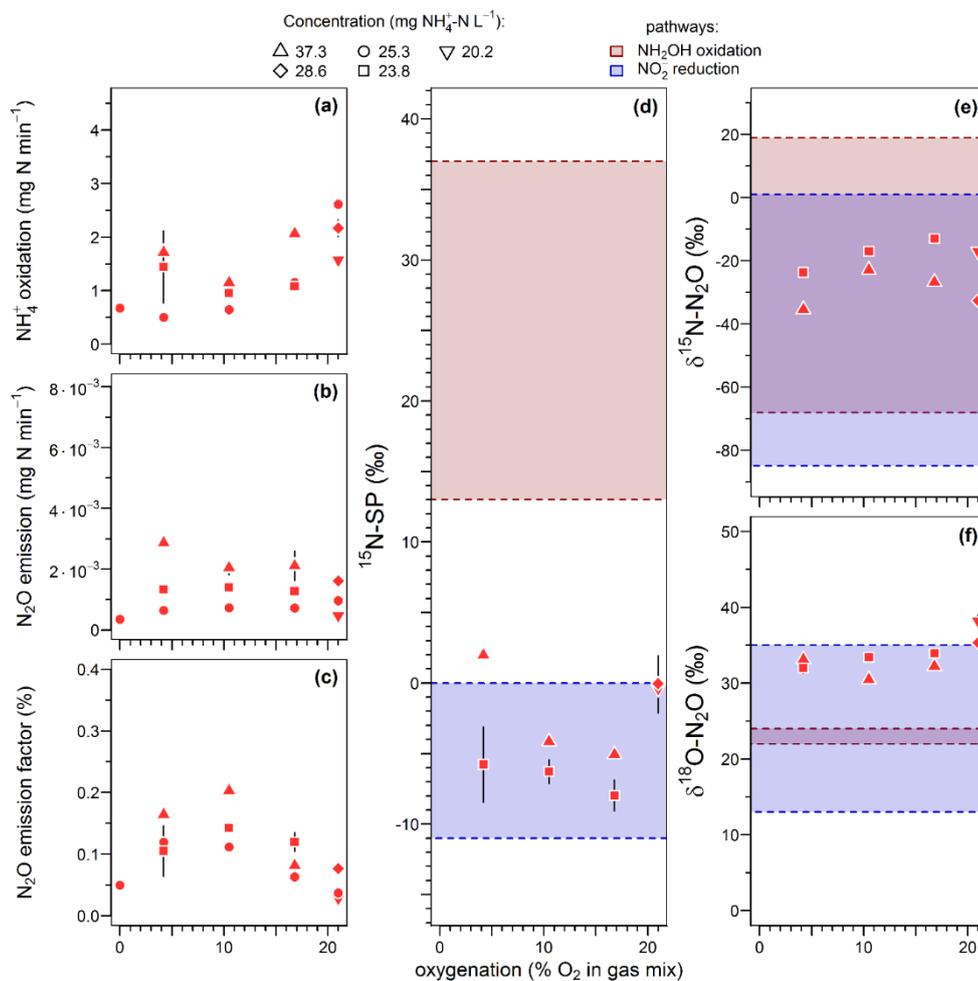
### 3.2 The effect of oxygen limitation on the N<sub>2</sub>O producing pathways

Ammonium concentrations decreased from 20.2-37.3 to 11.4-31.1 mg N L<sup>-1</sup>; with 45 to 89 % of the inflow ammonium  
225 remaining in the outflow during the oxygenation tests (Fig. S1d). The cumulated concentrations of NO<sub>2</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> ([NO<sub>x</sub><sup>-</sup>])  
increased from 2.4-4.1 to 4.7-11 mg N L<sup>-1</sup> between inflow and outflow and were composed by at least 74 and 82 % of NO<sub>3</sub><sup>-</sup>,  
respectively.

The oxygenation level had contrasting effects on ammonium oxidation rates, and N<sub>2</sub>O emission rates and factors (Figs. 3a-c).  
Between an oxygenation of 0 to 10.5 % O<sub>2</sub> in the gas mixture, ammonium oxidation rates were low and stable (1.1 ± 0.5 mg  
230 NH<sub>4</sub><sup>+</sup>-N min<sup>-1</sup>), with N<sub>2</sub>O emission rates and factors increasing from 0.35 10<sup>-3</sup> to 1.6 10<sup>-3</sup> mg N min<sup>-1</sup> and from 0.05 to 0.16 %,  
respectively. At oxygenation levels from 10.5 to 21 % O<sub>2</sub>, the ammonium oxidation rates increased from 0.9 ± 0.2 to 2.1 ± 0.4  
mg N min<sup>-1</sup>, with N<sub>2</sub>O emission rates remaining stable at 1.2 10<sup>-3</sup> ± 0.6 10<sup>-3</sup> mg N min<sup>-1</sup> and the emission factors decreasing  
from 0.15 ± 0.03 to 0.06 ± 0.03 %.

The <sup>15</sup>N-SP varied between -9 to 2 ‰ over the range of imposed oxygenation levels, with a marked increase when oxygenation  
235 increased from 16.8 to 21 % O<sub>2</sub> (Fig. 3d). A similar marked change in nitrogen and oxygen isotope ratios of N<sub>2</sub>O (decrease  
and increase, respectively) was observed when oxygenation increased from 16.8 to 21 % O<sub>2</sub> (Figs. 3e and f). The <sup>15</sup>N-SP values  
were close to the range of -11 to 0 ‰ reported for N<sub>2</sub>O produced by nitrifying or denitrifying bacteria (Toyoda et al., 2017;  
Yamazaki et al., 2014). This suggests an important contribution of the NO<sub>2</sub><sup>-</sup> reduction pathway to N<sub>2</sub>O emissions. The <sup>15</sup>N-SP  
dynamics between and variations within the oxygenation levels suggest a higher amount of N<sub>2</sub>O reduced to N<sub>2</sub> at 4.2 than 16.8  
240 % O<sub>2</sub>. The reduction of N<sub>2</sub>O to N<sub>2</sub> can increase the <sup>15</sup>N-SP of residual N<sub>2</sub>O (Mothelet et al., 2013). In heterotrophic denitrifying  
bacteria however, the nitrous oxide reductase involved in this reaction is highly sensitive to inhibition by oxygen (Betlach and  
Tiedje, 1981; Otte et al., 1996). This might explain the decrease in <sup>15</sup>N-SP from -3.8 ± 4.4 ‰ to -7.2 ± 1.7 ‰ when O<sub>2</sub> increased  
from 4.2 to 16.8 %. This is also consistent with a possible onset of anoxic microsites within the reactor biomass more likely at  
4.2 than 16.8 % O<sub>2</sub>. Finally, the N<sub>2</sub>O reduction to N<sub>2</sub> likely explains the overall decrease in N<sub>2</sub>O emission between 16.8 and 0  
245 % O<sub>2</sub> (Fig. 3b).

In general the N<sub>2</sub>O reduction to N<sub>2</sub> is accompanied by an increase in nitrogen and oxygen isotope ratios of N<sub>2</sub>O (Ostrom et al.,  
2007; Vieten et al., 2007). However, our results show a decrease in δ<sup>15</sup>N-N<sub>2</sub>O and the δ<sup>18</sup>O-N<sub>2</sub>O remained stable between 30.5  
and 34.7 ‰ when the N<sub>2</sub>O reduction is thought to increasingly constraint the N<sub>2</sub>O isotopocules with decreasing O<sub>2</sub> from 16.8  
to 4.2 % (Figs. 3e and f). The independence of samples taken during the oxygenation test can explain this. The N<sub>2</sub>O sampled  
250 at 4.2 % O<sub>2</sub> is not the N<sub>2</sub>O produced at 16.8 % O<sub>2</sub> then partially reduced. Before being reduced, the N<sub>2</sub>O produced at different  
oxygen levels has an isotope composition likely controlled by the reaction rates and the resulting net isotope effect. For  
example, Vieten et al. (2007) reported such control of isotope fractionation factors by the oxygenation levels through the  
control of N<sub>2</sub>O reduction rate. Additionally, with δ<sup>18</sup>O below 35 ‰ for all but one experiment the oxygenation tests did not  
provide evidence for denitrifier contribution to N<sub>2</sub>O emissions, likely due to oxygen-exchange with water (Snider et al., 2015,  
255 2012, 2013).



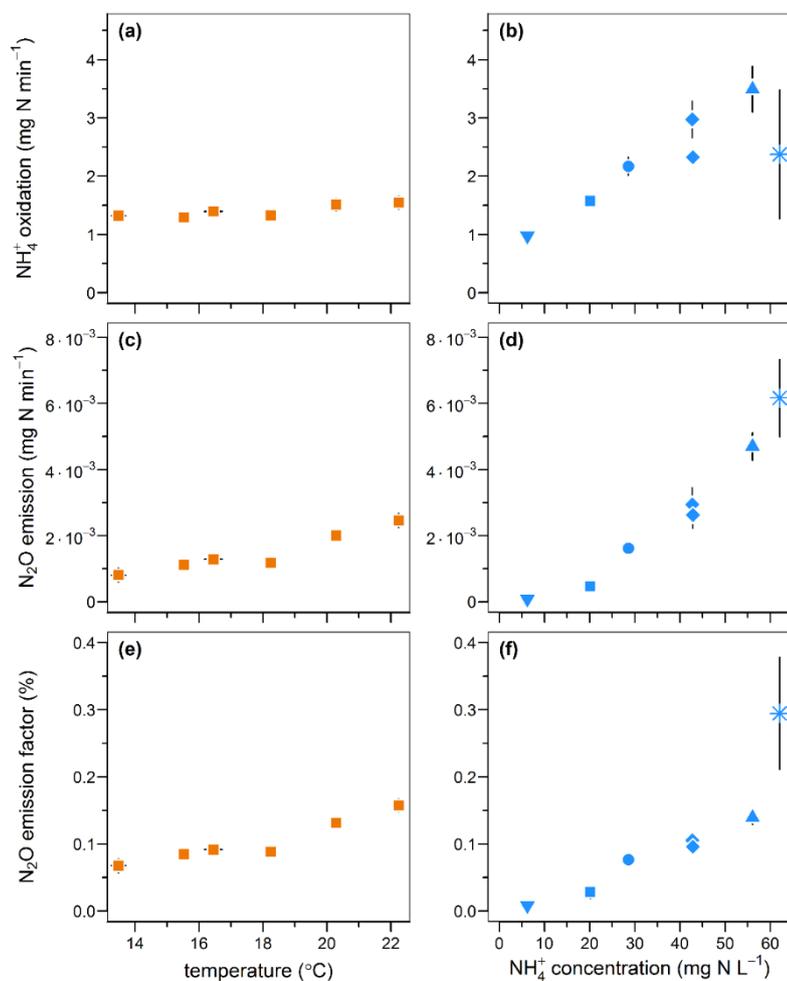
**Figure 3: Effect of oxygenation level on (a) the ammonium oxidation rate, (b) the nitrous oxide emission rate, (c) the N<sub>2</sub>O emission factor, and (d) the nitrogen isotopomer site preference, (e) the nitrogen isotope ratio, and (f) the oxygen isotope ratio of N<sub>2</sub>O. Average and standard deviation (error bars) are calculated for the steady-state conditions.**

### 3.3 Difference in temperature dependency of hydroxylamine and ammonium oxidizers as driver of hydroxylamine oxidation contribution to N<sub>2</sub>O emissions

Ammonium concentrations decreased from 6.2-62.1 to 0.9-54.1 mg N L<sup>-1</sup>; from 18 to 79 % of the inflow ammonium remaining in the outflow during the temperature and ammonium concentration tests (Figs. S1e and f). This remaining fraction was positively correlated to ammonium concentrations ( $r = 0.96$ ), and negatively correlated to temperature within the lower range of values (61-67 %;  $r = -0.94$ ). The cumulated concentrations of NO<sub>2</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> ([NO<sub>x</sub><sup>-</sup>]) increased from 1.4-6.1 to 5.1-19.6 mg N L<sup>-1</sup> between inflow and outflow and were composed by at least 74 and 91 % of NO<sub>3</sub><sup>-</sup>, respectively. Noticeably, the nitrite concentrations in the outflow linearly increased with temperature ( $r^2 = 0.95$ ; Fig. S1h).



An increase in temperature and inflow ammonium concentrations both positively influenced the rates of  $\text{NH}_4^+$  oxidation and  $\text{N}_2\text{O}$  emissions and the emission factor (Fig. 4). The  $\text{NH}_4^+$  oxidation rate linearly increased from 1.3 to 1.5  $\text{mg NH}_4^+\text{-N min}^{-1}$  with temperature ( $r = 0.89$ ; Fig. 4a) and increased from 0.97 to 3.49  $\text{mg NH}_4^+\text{-N min}^{-1}$  with a tenfold increase in the inflow ammonium concentration ( $r = 0.82$ ; Fig. 4b). These positive correlations are well known in the temperature range investigated here and are likely due to enhanced enzymatic activity (Groeneweg et al., 1994; Kim et al., 2008; Raimonet et al., 2017). Similarly, the  $\text{N}_2\text{O}$  emission rates increased from  $80.4 \cdot 10^{-6}$  to  $2.5 \cdot 10^{-3}$   $\text{mg N}_2\text{O-N min}^{-1}$ , and from  $83.6 \cdot 10^{-6}$  to  $6.2 \cdot 10^{-3}$   $\text{mg N}_2\text{O-N min}^{-1}$  upon changes in temperature and ammonium concentrations, respectively. These results are in agreement with positive correlations between  $\text{N}_2\text{O}$  emissions with temperature and ammonium concentration observed from modelling and experimental studies on partial nitrification and activated sludge systems (Guo and Vanrolleghem, 2014; Law et al., 2012a; Reino et al., 2017). Altogether this confirms a correlation between the  $\text{N}_2\text{O}$  emission rates and to the ammonium oxidation rates. Interestingly, the increase in  $\text{N}_2\text{O}$  emission factor indicates a stronger effect of temperature and ammonium concentration on the  $\text{N}_2\text{O}$  emission rate than on  $\text{NH}_4^+$  oxidation. The  $\text{N}_2\text{O}$  emission factors increased from 0.07 to 0.16 %, and from 0.01 to 0.29 % with temperature and inflow ammonium concentration, respectively ( $r > 0.94$ ; Figs. 4e and f). Both experiments suggest that the increase in  $\text{N}_2\text{O}$  emissions result from the increasing production of  $\text{N}_2\text{O}$  by hydroxylamine oxidation or nitrite reduction in combination with a slow rate of or absence of  $\text{N}_2\text{O}$  reduction to  $\text{N}_2$ . Furthermore, no nitrite accumulation was observed with increasing ammonium oxidation rate (Fig. S1i). Therefore, in the case where  $\text{N}_2\text{O}$  emission results mainly from the nitrite reduction pathway, this suggests that the nitrite reduction pathway is more responsive to the increasing ammonium oxidation rate than the nitrite oxidation pathway.



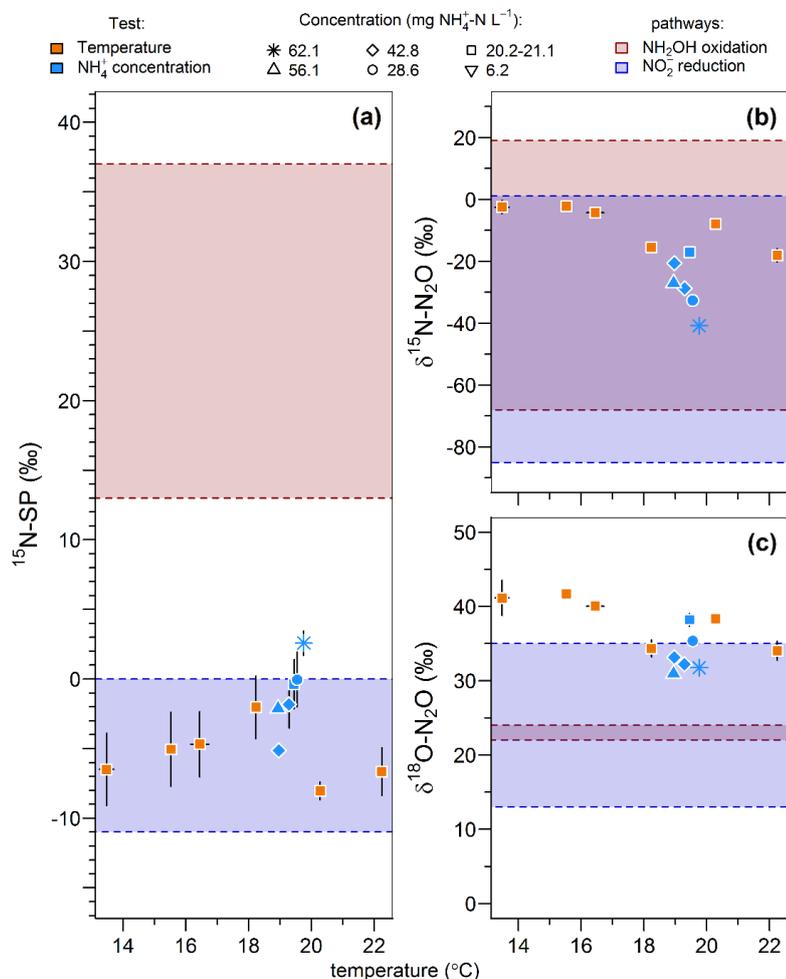
**Figure 4: Effect of temperature and inflow ammonium concentration on (a, b) the ammonium oxidation rate, (c, d) the nitrous oxide emission rate, and (e, f) the N<sub>2</sub>O emission factor.**

The range of nitrogen isotopomer site preference observed during the temperature and concentration tests (from -8 to 2.6 ‰) was similar to those measured during the oxygenation tests; confirming the high contribution of the nitrite reduction pathway to N<sub>2</sub>O emissions (Fig. 5a). This is consistent with previous findings based on the <sup>15</sup>N-SP of N<sub>2</sub>O emitted from aerobic activated  
285 sludge (Toyoda et al., 2011; Wunderlin et al., 2013). Furthermore, the <sup>15</sup>N-SP increased with temperature and ammonium concentration for temperatures between 13.5 and 19.8 °C. Similarly, Wunderlin et al. (2012, 2013) observed an increase in <sup>15</sup>N-SP from -1.2 to 1.1 ‰ when inflow [NH<sub>4</sub><sup>+</sup>] increased from 9 to 15 mg N L<sup>-1</sup>. They also observed 3-6 ‰ decreases in <sup>15</sup>N-SP over the course of ammonium oxidation experiments and suggested that NH<sub>2</sub>OH oxidation contribution to N<sub>2</sub>O production increased when conditions of NH<sub>4</sub><sup>+</sup> in excess, low NO<sub>2</sub><sup>-</sup> concentrations and high nitrogen oxidation rate occur simultaneously.  
290 Our data suggest that temperature mainly controlled the change in N<sub>2</sub>O producing pathways (Fig. 5a). This is consistent with the observation of Groeneweg et al. (1994) showing that temperature rather than ammonium concentration influenced the



ammonium oxidation rate. The  $^{15}\text{N}$ -SP increased from -6.5 to 2.6 ‰ with increasing temperature from 13.5 to 19.8 °C (Fig. 5a). This  $^{15}\text{N}$ -SP increase may either result from an increase in the  $\text{N}_2\text{O}$  production by the hydroxylamine oxidation pathway or the  $\text{N}_2\text{O}$  reduction to  $\text{N}_2$ . Since an optimal oxygenation level was imposed and increased emissions were observed, the increasing  $^{15}\text{N}$ -SP is more likely due to  $\text{N}_2\text{O}$  production by the hydroxylamine oxidation pathway. Reino et al. (2017) also observed an increase of  $\text{N}_2\text{O}$  emissions for temperature above 15 °C in a granular sludge airlift reactor performing partial nitrification. The authors suggested two hypothesis to explain their results: (i) the difference in the kinetic dependency with temperature of enzymes involved in ammonium and hydroxylamine oxidation; (ii) the temperature dependency of the acid-base equilibrium ammonium-ammonia. The changes in  $^{15}\text{N}$ -SP observed here are consistent with the former hypotheses. Hydroxylamine oxidation likely becomes the limiting step at a temperature above 15 °C, while being faster than ammonium oxidation at lower temperature (Fig. 6). At temperature above 15 °C, hydroxylamine therefore accumulates and leads to a higher contribution of the hydroxylamine oxidation pathway to  $\text{N}_2\text{O}$  emissions. It would thus be interesting to determine the temperature dependency of the hydroxylamine oxidase.

The change in nitrous oxide producing and consuming pathways had contrasted effects on the nitrogen and oxygen isotope ratios of nitrous oxide (Figs. 5b and c). The  $\delta^{15}\text{N}$ - $\text{N}_2\text{O}$  decreased from -2.5 to -40.9 ‰ with an increasing contribution of hydroxylamine oxidation to the  $\text{N}_2\text{O}$  emissions; i.e. when temperature increased from 13.5 to 19.8 °C. This is in contrast with the expected net lower isotope effect for  $\text{N}_2\text{O}$  produced by hydroxylamine oxidation than nitrite reduction and points out that further investigations are needed (Snider et al., 2015; Yamazaki et al., 2014). The changes in  $\delta^{18}\text{O}$ - $\text{N}_2\text{O}$  were less straightforward; likely influenced by changes in the reaction rates in addition to changes in the contribution of  $\text{N}_2\text{O}$  producing pathways. The values decreased from 41.1 to 34.3 ‰ with an increasing contribution of hydroxylamine oxidation to the  $\text{N}_2\text{O}$  emissions; when temperature increased from 13.5 to 18.2 °C. It decreased linearly from 38.2 to 31.8 ‰ with increasing reaction rate, when inflow ammonium concentration increased from 20.2 to 62.1 mg  $\text{NH}_4^+\text{-N L}^{-1}$  ( $r^2 = 0.83$ ).



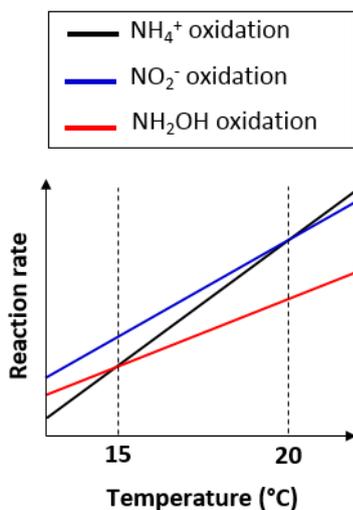
**Figure 5: Effect of temperature (orange symbols) and inflow ammonium concentration (blue symbols) on (a) the nitrogen isotopomer site preference, (b) the nitrogen isotope ratio, and (c) the oxygen isotope ratio of N<sub>2</sub>O. Average and standard deviation (error bars) are calculated for the steady-state conditions.**

### 3.4 Difference in oxidation and reduction rates of nitrite as driver of nitrite reduction contribution to N<sub>2</sub>O emissions

The oxygenation, temperature and ammonium concentration tests revealed a strong control of nitrite oxidizing activity and the contribution of the nitrite reduction pathway to N<sub>2</sub>O production. During the oxygenation test, the combination of stable NO<sub>2</sub><sup>-</sup> concentrations and higher <sup>15</sup>N-SP at 21 % compared to the 10.5-16.8 % O<sub>2</sub> was observed while temperature remained below 20 °C (Figs. S1g and 3d). This is most likely due to higher nitrite oxidation than nitrite reduction rates in response to increasing oxygenation levels to 21 % O<sub>2</sub>, which is consistent with the nitrite oxidation step sensitivity to oxygen limitation (Pollice et al., 2002; Tanaka and Dunn, 1982). Additionally, the <sup>15</sup>N-SP close to 0 ‰ observed at the highest oxygenation level indicates a decreasing contribution to N<sub>2</sub>O production of nitrite reduction over hydroxylamine oxidation pathway. The highest



oxygenation level thus limits the reduction pathways (i.e.  $\text{NO}_2^-$  reduction to  $\text{N}_2\text{O}$  and  $\text{N}_2\text{O}$  reduction to  $\text{N}_2$ ) while favoring the ammonium and nitrite oxidation pathways.



**Figure 6: Scheme of the difference in temperature dependency of the reactions involved in nitrification.**

During the temperature and ammonium concentration tests, the contribution of the hydroxylamine oxidation pathway to  $\text{N}_2\text{O}$  emissions exponentially increased with temperature between 15 and 20 °C (Sect. 3.2) and decreased in favor of the nitrite reduction pathway when temperature exceeded 20 °C (Fig. 5a). The  $^{15}\text{N}$ -SP was low when temperature exceeded 20 °C ( $-7.3 \pm 1 \text{ ‰}$ ), while being higher than  $-5 \text{ ‰}$  ( $-1.3 \pm 2.4 \text{ ‰}$ ) when temperature ranged from 18.2 to 19.8 °C. At temperatures above 20 °C, ammonium oxidation rates exceeded nitrite oxidation rates (Fig. 6; Kim et al., 2008; Raimonet et al., 2017). This explains most likely the increased contribution of the nitrite reduction pathway to  $\text{N}_2\text{O}$  emission, as more nitrite becomes available for nitrifier-denitrification and/or denitrification. As little nitrite accumulated (Fig. S1h), lower rates of nitrite consuming than producing processes can be inferred (nitrite reduction and oxidation vs. ammonium oxidation). Additionally, values of  $\delta^{18}\text{O} > 35 \text{ ‰}$  measured during these tests suggest a significant contribution of denitrifiers to  $\text{N}_2\text{O}$  emissions (Snider et al., 2013). This seems to occur at the lowest hydroxylamine oxidation contribution to  $\text{N}_2\text{O}$  production; below 18°C and at 20.3 °C. Furthermore, the denitrifiers were impacted to a larger extent by temperature than ammonium concentration.

#### 4 Conclusion

Our results demonstrated that whatever the imposed conditions, the nitrifying biomass produced  $\text{N}_2\text{O}$  and nitrite reduction remained the main  $\text{N}_2\text{O}$  producing pathway. The  $\text{N}_2\text{O}$  emissions were sensitive to oxygenation, temperature, and  $\text{NH}_4^+$  concentration likely due to control of enzymatic activities. The use of  $\text{N}_2\text{O}$  isotopocules confirmed the processes that control  $\text{N}_2\text{O}$  emissions under oxygenation constrain and improved the knowledge of processes that control  $\text{N}_2\text{O}$  under temperature constrain. Among the environmental variables tested, temperature appears to be the main control on  $\text{N}_2\text{O}$  producing pathways



340 under nitrifying conditions, due to its dissimilar effects on ammonium and nitrite oxidizing activities. Ranges of optimal temperature for nitrification and limited N<sub>2</sub>O emissions can be recommended. The combination of low N<sub>2</sub>O emissions and high nitrification rates would occur close to 15 °C. From 15 to 20 °C, increasing nitrification rate increase the N<sub>2</sub>O emissions by the hydroxylamine oxidation pathway. Above 20 °C, an increasing nitrification rate increases the N<sub>2</sub>O emissions via the nitrite reduction pathway.

#### 345 **Supplementary material**

Additional information about the nitrifying activity of the biomass, the experimental conditions, and the time series of ammonium oxidation experiments.

#### **Author contribution**

JF, AF and MSp designed the experiments with contributions from GH, MSe and AML. GH, JF and LL carried the experiments  
350 out. GH performed the stable isotope measurements with contribution from VV and interpreted them with contribution from MSe. GH and JF processed the data. GH, JF and AML prepared the manuscript with contributions from all co-authors.

#### **Competing interests**

The authors declare that they have no conflict of interest.

#### **Acknowledgements**

355 This work is part of the ‘N<sub>2</sub>OTrack’ project ANR-15-CE04-0014-02 funded by the French National Research Agency. Furthermore, the authors are grateful to Sam Azimi and the ‘Direction Innovation Environment’ of SIAAP for providing the media colonized by the nitrifying biomass, Mansour Bounouba and Simon Dubos for their assistance in chemical analyses and in setup and development of the nitrifying reactor.

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